

Thermal analysis on the Li–Mg–B–H systems

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Abstract

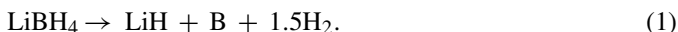
Thermal analyses of the mixture of MgH₂ and LiBH₄ doped with TiCl₃, and each element MgH₂ or LiBH₄ doped with TiCl₃ were performed under an inert gas flow and 0.5 MPa H₂-gas conditions. It was indicated that the hydrogen desorption reaction of MgH₂ + 2LiBH₄ to MgB₂ + 2LiH + 4H₂ phases proceeded at temperature above 400 °C under 0.5 MPa hydrogen, whereas, under an inert gas atmosphere, the reaction of the same mixture was transformed into Mg + 2B + 2LiH + 4H₂ phases in a temperature range from 350 to 430 °C. Before these reactions, the dehydrogenation of MgH₂ and the melting of LiBH₄ took place under both hydrogen and the inert gas atmospheres with increasing temperature. In addition, the molten LiBH₄ did not decompose into LiH, B and H₂ below 450 °C under 1 MPa H₂, while the LiBH₄ decomposed even below 450 °C under an inert gas atmosphere. From these results, it is deduced that the reaction producing MgB₂ is a solid–liquid reaction between solid Mg and liquid LiBH₄ above 400 °C without decomposition of molten LiBH₄ under a hydrogen atmosphere, while MgH₂ dehydrogenate. A characteristic solid–liquid reaction is realized under a hydrogen atmosphere for proceeding of the MgB₂ producing reaction in this system.

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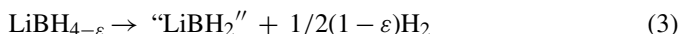
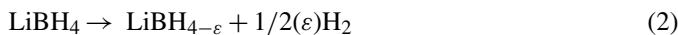
Keywords: Hydrogen storage materials; Liquid–solid reactions; X-ray diffraction; Thermal analysis

1. Introduction

Lithium borohydride (LiBH₄) is one of the most attractive candidates for hydrogen storage because of its high gravimetric and volumetric hydrogen densities; about ~18 mass% and 121 kg H₂/m³, respectively [1]. The synthesis of pure LiBH₄ was firstly performed in 1940 by Schlesinger and Brown [2] and the thermal analysis of LiBH₄ was performed in 1964 by Fedneva et al. [3]. However, this material had not been paid attention as a hydrogen storage material until 21st Century. The first investigation of LiBH₄ as a hydrogen storage material was reported by Züttel et al. [4,5] in which thermal decomposition properties were examined. They reported that LiBH₄ desorbed hydrogen up to ~13.5 mass% according to the following reaction:



However, the dehydrogenating temperature of LiBH₄ was too high for practical use and the reversibility was not realized because of its quite slow kinetics. At the next step, they reported that the thermal decomposition of SiO₂-doped LiBH₄ has three dehydrogenation steps on LiBH₄ with increasing temperature as follows:



Recently, many researchers have focused on this system [6–8]. Among them, Orimo et al. reported that the rehydrogenation reaction of LiH and B proceeded to form LiBH₄ under 35 MPa H₂-gas pressures at 600 °C [9].

In 2004, two independent groups developed a new hydrogen storage system composed of LiBH₄ and magnesium hydride (MgH₂), which exhibited a much better reversibility than LiBH₄ itself [10–12]. The reaction is expressed as follows:



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It is noteworthy that a finite hydrogen pressure is necessary for the reaction of Mg with LiBH_4 to yield MgB_2 . In contrast, the Mg and B phases instead of the MgB_2 phase are produced after dehydrogenation under vacuum. This reaction is expressed as follows:



At present, it is not yet clear which role the hydrogen atmosphere does play in the reaction (5). Therefore, in this paper, we report on the results of thermal analysis for the mixture of MgH_2 and LiBH_4 under different atmospheric conditions. And finally, we try to clarify the role of hydrogen in this system.

2. Experimental

In this work, MgH_2 powder (95 mass% purity, Gelest Inc.), LiBH_4 powder (95 mass% purity, Sigma–Aldrich) and titanium chloride powder (TiCl_3 , 99.999 mass% purity, Sigma–Aldrich) were used as starting materials. Thermal analyses were performed for MgH_2 , LiBH_4 and a mixture of MgH_2 and 2LiBH_4 , in which 3 mol% TiCl_3 was added as a catalyst. Prior to thermal analyses, all the samples were ball-milled by a planetary ball-mill apparatus (Fritsch P7) for 2 h at 400 rpm under 1.0 MPa highly pure hydrogen gas (7N). Mixed powders of ~ 300 mg and 20 pieces of steel balls with a diameter of 7 mm were loaded into the milling container (Cr–steel pot with an internal volume of ~ 30 ml). The thermal analyses were examined by a pressurized differential scanning calorimetry (p-DSC) (TA Instruments, DSC Q10P) and a thermogravimetry with differential thermal analysis equipment (TG-DTA) (Rigku, TG8120). The measurement of p-DSC was operated under ~ 0.3 MPa Ar gas flow, or under 0.5 MPa H_2 gas as initial pressure (final pressure at 450°C was ~ 0.7 MPa) in a closed system, while the TG-DTA measurement was operated under a He gas flow condition. The heating rate was fixed at $5^\circ\text{C}/\text{min}$ for both measurements. The identification of the products was carried out by X-ray powder diffraction (XRD) measurements (Rigaku, RINT-2500, Cu $\text{K}\alpha$). All the processes from the sample preparation to the thermal analyses were performed in Ar-filled gloveboxes with a recycling purification system (MP-P60W, Miwa MFG Co., LTD) to avoid the sample pollutions by water vapor and oxygen (the dew point of water was lower than -80°C and the oxygen concentration was below 1 ppm).

3. Result and discussion

The thermal analyses for the TiCl_3 -doped MgH_2 and the TiCl_3 -doped LiBH_4 are shown in Figs. 1 and 2, respectively.

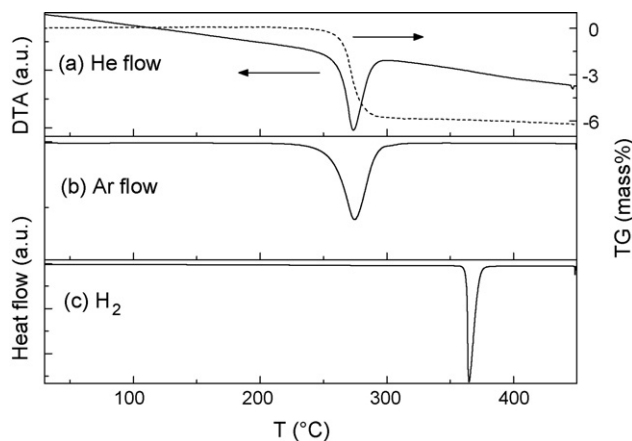


Fig. 1. TG-DTA and DSC profiles of TiCl_3 -doped MgH_2 . (a) TG-DTA profile under a He flow, (b) DSC profile under an Ar flow and (c) DSC profile under 0.5 MPa H_2 (initial pressure).

The thermal analyses were performed by TG-DTA under a He gas flow, p-DSC under ~ 0.3 MPa Ar gas flow and 0.5 MPa H_2 -gas in the closed system. It can be seen that the decomposition temperature of the TiCl_3 -doped MgH_2 is $\sim 280^\circ\text{C}$ under the He-gas flow (Fig. 1(a)), which is almost the same as that of under the Ar flow condition (Fig. 1(b)), irrespective of sorts of inert gases. This result indicates that an inert gas gives no influence on the dehydrogenation properties of MgH_2 . On the other hand, in the p-DSC profile under 0.5 MPa H_2 gas pressure (Fig. 1(c)), an endothermic peak corresponding to decomposition of MgH_2 is observed at higher temperature ($\sim 370^\circ\text{C}$) than that under the inert gas flow, where the pressure rises to ~ 0.6 MPa at this temperature. This indicates that the hydrogen dissociation pressure is about 0.6 MPa at $\sim 370^\circ\text{C}$, suppressing the dehydrogenation of MgH_2 by a reverse reaction.

For LiBH_4 doped with a small amount of TiCl_3 , three endothermic reactions are observed in the DTA profile under a He gas flow (Fig. 2(a)), which is almost the same as under an Ar flow condition as shown in Fig. 2(b). Therefore, the inert gases do not show any differences on the dehydrogenation properties of LiBH_4 . Here, it should be noted that the measuring temperature was limited up to 450°C , because the sample pan of the Al metal was used in this work. For this reason, unfortunately, the third reaction peak could not be clearly observed in the DTA or DSC profiles under the inert gases, but the endothermic reactions could be recognized above 400°C since the DSC signals are lower than the base lines. Comparing with the results reported by Fedneva et al. [3] and Soulié et al. [13], three endothermic reactions in Fig. 2(a) and (b) correspond to the phase transition ($\sim 105^\circ\text{C}$, orthorhombic to hexagonal), the melting phenomenon ($\sim 280^\circ\text{C}$) and the decomposition into LiH, B and H_2 (above 400°C). On the other hand, under 0.5 MPa H_2 gas pressure in Fig. 2(c), two endothermic peaks are observed below 300°C , but there is no other reaction above 300°C . These two peaks are recognized at the same temperatures as those under the inert gas conditions, indicating that the hydrogen pressure does not affect both the temperatures of phase transition and melt of LiBH_4 . However, the third reaction above 300°C disappears in the DSC profile under 0.5 MPa H_2 gas pressure, where

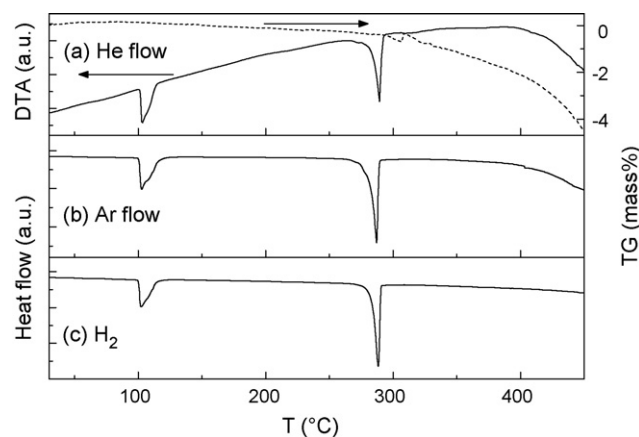


Fig. 2. TG-DTA and DSC profiles of TiCl_3 -doped LiBH_4 . (a) TG-DTA profile under a He flow, (b) DSC profile under an Ar flow and (c) DSC profile under 0.5 MPa H_2 (initial pressure).

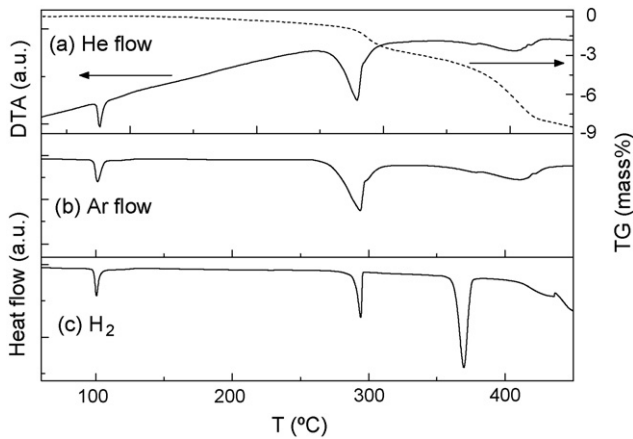


Fig. 3. TG-DTA and DSC profiles of TiCl_3 -doped mixture of MgH_2 and 2LiBH_4 . (a) TG-DTA profile under a He flow, (b) DSC profile under an Ar flow and (c) DSC profile under 0.5 MPa H_2 (initial pressure).

the pressure rises to ~ 0.7 MPa at 450°C . These results indicate that the hydrogen dissociation pressure of LiBH_4 is lower than 0.7 MPa at 450°C , suppressing the dehydrogenation of LiBH_4 by the H_2 absorption process.

Fig. 3 shows a TG-DTA profile under a He gas flow and p-DSC profiles under ~ 0.3 MPa Ar gas flow and 0.5 MPa H_2 gas pressure for the TiCl_3 -doped mixture of MgH_2 and 2LiBH_4 . Under an inert gas conditions in Fig. 3(a) and (b), there are three endothermic peaks at ~ 105 , ~ 280 and $\sim 410^\circ\text{C}$, respectively. The two peaks below 350°C are identified with similarity to above results as the phase transition of LiBH_4 ($\sim 105^\circ\text{C}$) and superposition of the melt of LiBH_4 and dehydrogenation of MgH_2 ($\sim 280^\circ\text{C}$), whereas, the endothermic peak at $\sim 410^\circ\text{C}$ is due to the dehydrogenation of LiBH_4 . Actually, LiH and Mg phases were confirmed in the X-ray profile (Fig. 4(b)) of the product after the DSC measurement at 450°C under the Ar gas flow condition. Under 0.5 MPa H_2 gas pressure in Fig. 3(c), four endothermic reactions were observed around ~ 105 , ~ 280 , ~ 370 and above 400°C . The first and the second reactions (the peaks at ~ 105 and $\sim 280^\circ\text{C}$) are due to the phase transition and melt of LiBH_4 because these peak temperatures are almost the same as those in Fig. 2(c). The third peak temperature at $\sim 370^\circ\text{C}$ is similar to that of the peak in Fig. 1(c), so that the third reaction is due to the decomposition of MgH_2 . Actually, the Mg phase is observed in the XRD profile as shown in Fig. 4(d) later, which was examined after heating the product up to 380°C under 0.5 MPa H_2 gas pressure. Here, it should be noted that the most important point is appearance of the fourth endothermic peak above 400°C . This peak was neither observed in the case of DSC measurement of MgH_2 nor LiBH_4 under 0.5 MPa H_2 pressure. This indicates that the dehydrogenation reaction depends on the difference whether hydrogen pressure is applied or not on the dehydrogenation process.

Fig. 4 shows XRD patterns of TiCl_3 -doped mixture of MgH_2 and 2LiBH_4 . When a hydrogen pressure of 0.5 MPa was applied in a dehydrogenation process, the two phases of MgB_2 and LiH were produced (Fig. 4(c)). On the other hand, when no hydrogen pressure, such as an inert gas atmosphere, is applied, three phases of Mg, B and LiH were produced (Fig. 4(b)). Unfortunately,

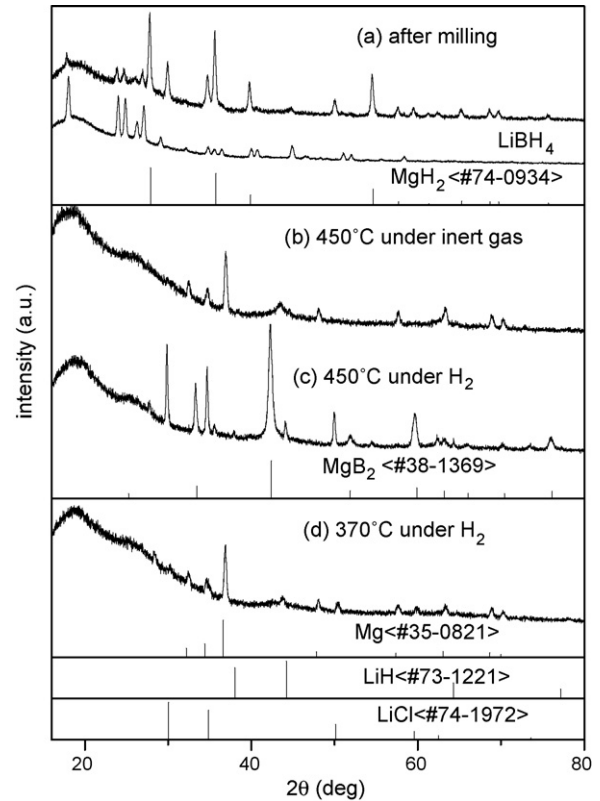


Fig. 4. XRD patterns of TiCl_3 -doped mixture of MgH_2 and 2LiBH_4 . (a) After milling, (b) after heat treatment under an inert gas flow at 450°C , (c) after heat treatment under 0.5 MPa H_2 (initial pressure) at 380°C and (d) after heat treatment under 0.5 MPa H_2 (initial pressure) at 450°C .

we could not find any peaks originated from B related phases, because the B peaks corresponding to single phase are too weak to be observed in our experiment. Therefore, it was clarified that the MgB_2 was generated in the forth reaction (above 400°C).

From the above results, we conclude that the reaction (5) proceeds in hydrogen pressure without the decomposition of LiBH_4 , though LiBH_4 is under the molten phase at the temperature above 400°C with Mg. This result indicates that the suppression of the LiBH_4 decomposition by hydrogen pressure plays the important role in the proceeding of the reaction (5). In addition, the reaction (5) proceeds by a solid–liquid reaction between the solid Mg phase and molten LiBH_4 phase, where the liquid phase of LiBH_4 leads to a much better contact with Mg and the Li^+ and $(\text{BH}_4)^-$ ions than a solid–solid reaction. This reaction is different from other typical hydrogen storage systems, so that this system may exhibit a characteristic reaction. In addition, hydrogen gas atmosphere could bring another contribution for proceeding of a direct reaction between condensed materials just like Mg and LiBH_4 . As suggested by Hayashi et al., hydrogen in materials introduces some defects and reduces activation barriers for the mobility of atoms [14]. Similarly, some defects in the composite mixture of Mg and LiBH_4 could be introduced by exchanging hydrogen between the gas phase and condensed phase, and the activation barriers for the mobility of atoms in the composite mixture of Mg and LiBH_4 might be reduced, possibly yielding MgB_2 and LiH in this system.

4. Summary

In this work, we performed the thermal analyses of the TiCl_3 -doped mixture of MgH_2 and LiBH_4 , and each element MgH_2 or LiBH_4 doped with TiCl_3 under an inert gas flow and 0.5 MPa H_2 -gas conditions. The results indicated that the reaction $[2\text{LiBH}_4 + \text{MgH}_2 \rightarrow 2\text{LiH} + \text{MgB}_2 + 4\text{H}_2]$ proceeded at 450 °C under hydrogen atmosphere of 0.5 MPa, whereas, the reaction $[2\text{LiBH}_4 + \text{MgH}_2 \rightarrow \text{Mg} + 2\text{B} + 2\text{LiH} + 4\text{H}_2]$ was induced under the inert gas atmosphere. This indicated that MgB_2 was produced by the solid–liquid reaction between solid Mg and liquid LiBH_4 at temperature above 400 °C, where the molten LiBH_4 phase remained without the dehydrogenation into $\text{B} + \text{LiH} + 1.5\text{H}_2$ under hydrogen atmosphere, while MgH_2 was dehydrogenated. Probably, a characteristic reaction between Mg metal and $(\text{BH}_4)^-$ ion was realized in this solid–liquid reaction system.

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